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QUERY CONTROL FORM		RTIS USE ONLY	
Application No.	09/841,654	Prepared by	NPB
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## JACKET

a. Serial No.	f. Foreign Priority	k. Print Claim(s)	① PTO-1449
b. Applicant(s)	g. Disclaimer	l. Print Fig.	q. PTOL-85b
c. Continuing Data	h. Microfiche Appendix	m. Searched Column	r. Abstract
d. PCT	i. Title	n. PTO-270/328	s. Sheets/Figs
e. Domestic Priority	j. Claims Allowed	o. PTO-892	t. Other

<b>SPECIFICATION</b>	<b>MESSAGE</b>	
	In claim pages dated 06/17/04, original claim 125 (now claim 76) depends from original claim 137 (now 88).	
	Please advise/correct claim dependency.	
<b>CLAIMS</b>	initials <i>Amh</i>	
<b>RESPONSE</b>	initials <i>Amh</i>	

wt% of at least one metal selected from the group consisting of ruthenium, rhodium, iridium, titanium, magnesium, cobalt, copper, vanadium, manganese, niobium, and iron;

feeding liquid benzene to the reaction zone;

feeding nitrous oxide to the distillation zone;

contacting the benzene and the oxidant gas with the oxidation catalyst under

oxidation conditions effective to catalytically hydroxylate at least a portion of the benzene to produce hydroxylated product comprising phenol, the oxidation conditions comprising a temperature of from above 100°C to 270°C and a benzene partial pressure in the range of from about 0.1 atm to about 45 atm;

separating liquid phenol from the distillation zone.

124. (New) The process of claim 123 wherein the temperature of the distillation zone is higher than the boiling point of benzene and lower than the boiling point of phenol.

125. (New) The process of claim 127 wherein the at least one metal comprises iron.

126. (New) The process of claim 125 wherein the zeolite catalyst comprises from about 0.1 wt. % iron to about 1.0 wt. % iron.

127. (New) The process of claim 126 wherein the zeolite is an alumino-silicate produced without addition of boron.

128. (New) The process of claim 123 wherein the separating liquid phenol from the distillation zone comprises substantially continuous fractional distillation.

129. (New) The process of claim 127 wherein the separating liquid phenol from the distillation zone comprises substantially continuous fractional distillation.

130. (New) The process of claim 123 wherein the oxidation conditions comprise a temperature of from about 185 °C. to about 270 °C.

131. (New) The process of claim 129 wherein the conditions comprise a temperature of from about 185 °C. to about 270 °C.

132. (New) The process of claim 123 wherein selectivity for conversion of the oxidant gas to hydroxylated product is at least 90 mol %.